

## Ammonia as an Efficient Hydrogen Vector: Catalytic Pathways, Reactor Concepts and System Integration

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### Introduction

The transition toward low-carbon energy systems requires hydrogen delivery pathways that are not only clean at the point of use but also practical for storage, transport, and large-scale deployment. In this context, ammonia (NH<sub>3</sub>) emerges as a particularly attractive hydrogen vector because it combines a high hydrogen content, established industrial logistics, and comparatively mild liquefaction conditions [1-3]. Its role is especially compelling for distributed energy systems, maritime applications, and sectors where direct hydrogen handling remains technically burdensome [2-4]. This study examines ammonia not simply as a chemical commodity, but as an enabling intermediary for future hydrogen infrastructure.

### Materials and methods

The study is based on a critical survey of recent peer-reviewed literature addressing the full ammonia-to-hydrogen value chain. The analysis covers ammonia synthesis and logistics, catalyst and reactor engineering for NH<sub>3</sub> cracking, H<sub>2</sub> separation and purification, as well as techno-economic and environmental assessments. Particular attention is given to catalyst design, reaction pathways, operating temperature windows, reactor intensification strategies, and the compatibility of the resulting hydrogen with fuel-cell-grade specifications.

### Results and discussion

The literature shows that ammonia cracking is a favorable route for hydrogen generation [5, 6], yet its practical implementation is constrained by kinetic limitations, heat-transfer demands, catalyst stability, and product purification requirements. Ruthenium-based systems remain highly active [7, 8], but their cost motivates the development of earth-abundant alternatives based on nickel, cobalt, and iron [6-9], together with bimetallic formulations, tailored supports, and nanostructured architectures. In parallel, reactor concepts such as membrane reactors, microreactors, fluidized beds, and plasma-assisted systems [10-12], can improve conversion efficiency and reduce downstream separation burden. The integration of hydrogen-selective membranes is particularly promising because it enables in situ separation of H<sub>2</sub>, shifts equilibrium toward higher conversion, and supports continuous operation at lower effective temperatures [10, 11]. From a systems perspective, the overall attractiveness of ammonia increases when the upstream production route is decarbonized and when the cracking unit is coupled with renewable electricity, compact purification trains, and robust thermal management. Figure 1 illustrates NH<sub>3</sub> as a sustainable and carbon-free energy vector in the energy revolution. Techno-economic studies further indicate that the feasibility of ammonia-based hydrogen supply depends strongly on catalyst lifetime, scale, energy input, and infrastructure reuse [3]. Table 1 shows a comparative performance of catalysts for ammonia decomposition toward hydrogen production [6-9].

### Conclusions

Ammonia can serve as a credible bridge between hydrogen production and end use, provided that catalytic activity, durability, reactor integration, and purification efficiency continue to improve. The most viable near-term route is likely to combine optimized catalysts with membrane-assisted cracking and flexible heat supply,

thereby enabling fuel-cell-grade hydrogen from a transportable carbon-free carrier. Future progress will depend on coordinated advances in materials design, process intensification, and system-level integration.

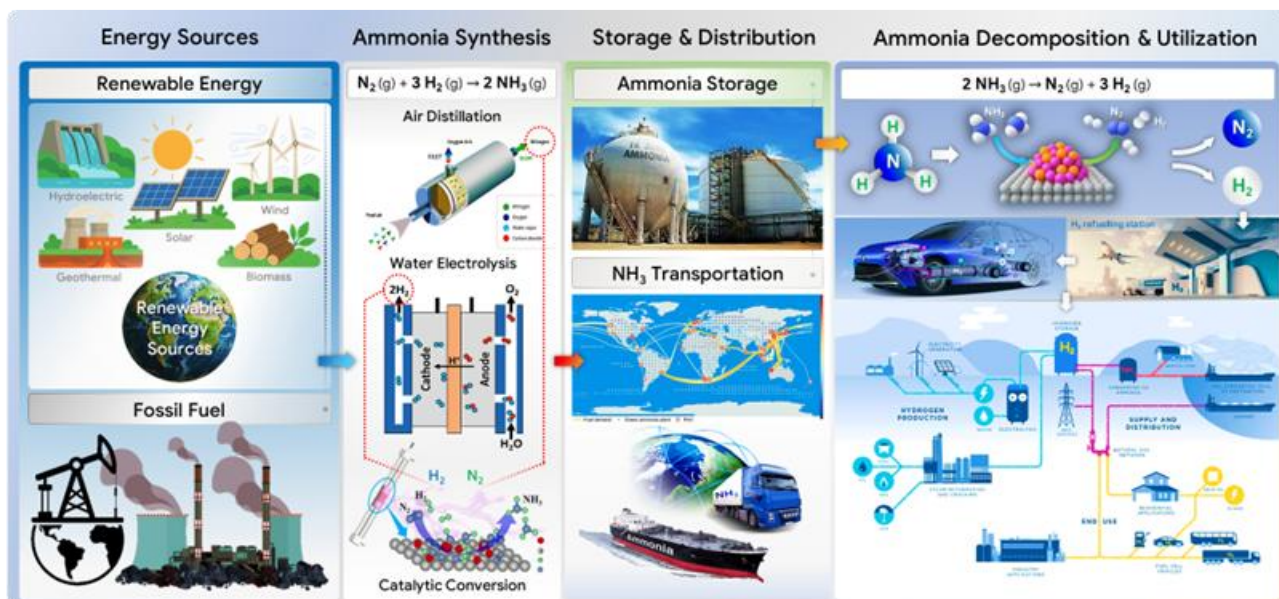


Figure 1. Ammonia as a sustainable and carbon-free energy vector in the energy revolution.

Table 1. Comparative performance of catalysts for ammonia decomposition toward hydrogen production [6-9].

Catalyst System	Active Phase	Temperature (°C)	Conversion (%)	Key Advantages	Limitations
Ru-based	Ru/Al <sub>2</sub> O <sub>3</sub> , Ru/CNT	400–600	~100	Highest activity, low temperature operation	High cost, scarcity
Ni-based	Ni/Al <sub>2</sub> O <sub>3</sub> , Ni-MgO	500–800	80–95	Low cost, scalable	Higher temperature required
Co-based	Co/SiO <sub>2</sub> , Co spinels	550–750	70–90	Moderate cost, good stability	Lower activity than Ni
Fe-based	Fe catalysts	600–800	60–85	Abundant, inexpensive	Kinetic limitations
Bimetallic	Ni-Ru, Co-Ni	450–700	85–98	Synergistic effects, improved stability	Synthesis complexity

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